Performance Optimization of Four Stage Cascade Refrigeration Systems using Energy-Exergy Analysis in the R1234ze & R1234yf in High Temperature Circuitand Ecofriendly Refrigerants in Intermediate Ciircuits and Ethane in the Low Temperature Circuit for Food, Pharmaceutical, Chemical Industries

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Abstract

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1. Introduction

Low-temperature refrigeration systems are typically required in the temperature range from -30°C to -100°C for applications in food, pharmaceutical, chemical, and other industries. At such low temperatures, single-stage compression systems with reciprocating compressors are generally not feasible due to high pressure ratios. A high pressure ratio implies high discharge and oil temperatures and low volumetric efficiencies and, hence, low COP values. Cascade refrigeration systems can be used to achieve low temperatures, where series of single-stage units thermally are used that are coupled through evaporator/condenser cascades. Each circuit has a different refrigerant suitable for that temperature. The hightemperature circuit uses high boiling point refrigerants such as R-1234ze, and R1234yf and Intermediate circuits thirteen ecofriendly refrigerants such as R-134a, R123, R125, HFC blends (R-507a), ammonia, propane, propylene, hydrocarbons, etc., whereas the low-temperature circuit uses low boiling refrigerants such as ethane. air, methane etc In a vapour compression cascade refrigeration system where low pressure vapour in the evaporator stage is compressed and then recycled for condensation in the evaporator of a previous stage, the improvement of passing the low pressure refrigerant's vapour from an evaporator stage through a heat exchanger to heated vapour to ambient temperature, compressing said heated vapour, removing the compressor work by passing said compressed vapour through a evaporator, then cooling is by compressed vapour by passing it through heat exchanger in heat exchanger at a low pressure vapour, and condensing it in the evaporator of the next higher temperature cycle of the cascade system and

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This paper mainly deals with the exergy analysis of Four stages cascade refrigeration systems used for low temperature applications using ecofriendly refrigerants. The effect of performance parameters (i.e. approaches, condenser temperature, and temperature variations in the evaporators) on the thermal performances in terms of second law efficiency of the system (exergetic efficiency) and exergy destruction ratio (EDR) and first law efficiency (i.e. overall coefficient of performance) have been optimized thermodynamically using of R1234yf and R1234ze in the high temperature circuits and mainly thirteen ecofriendly refrigerants in the intermediates circuits and ethane It was observed that in the low temperature (between- 80 °C to -88 °C) applications. It was observed that the best combination in terms of R1234ze-R134a-R410aethane gives better thermal performance than using R1234yf-R134a-R410aethane.

> recycling the liquid to the low pressure evaporator stage. Most of the investigators even did not find out the effect of various approaches on the system performances on three and four stages cascade refrigeration systems and effect of ecofriendly refrigerants in the primary intermediate temperature circuit and secondary intermediate temperature circuit. This paper mainly deals with thermal performances in terms of exergy destruction ratio by thermodynamically analyzing the use of R1234yf and R1234ze in the high temperature circuits and mainly thirteen eco-friendly refrigerants in the intermediates circuits and Ethane in the low temperature applications.

2. Literature Review

Agnew et al ^[1] examined the performance of a three stage cascade refrigeration systems. Arora et al^[2] analysis of a vapour compression refrigeration system with R502, R404A and R507. Bansal P.K^[3] did thermodynamic analysis of carbon dioxide-ammonia (R744-R717) cascade refrigeration system. Bhattacharyya et al [4] studied the performance of a cascade refrigeration-heat pump system based on a model incorporating both internal and external irreversibility's. Cabell et al ^[5] Made a simplified steadystate modeling of a single stage vapors compression plant.. Calm^[6] reviewed the progression of refrigerants Ecir et al ^[7] used ten modeling techniques within data mining process for the prediction of thermo-physical properties of refrigerants. Jain et al ^[10] showed that carbon dioxide is a potential low temperature refrigerant. Kilicarslan ^[12] experimental investigation and theoretical study of a different type of two-stage vapor compression cascade system. Lee et al ^[13] studied refrigeration thermodynamically a cascade refrigeration system that uses carbon dioxide and ammonia as refrigerants. Monte [14] calculated thermodynamic properties of R407C Pearson [16]

traced the development of the old carbon dioxide systems Samant [18] design and development of two stage cascade refrigearation system using CO2 as LTC refrigerant and Propane as HTC refrigerant. Resat S. et al [17] exergy based thermo-economic optimization of subcooled and superheated vapour compression refrigeration cycle. Wang et al [18] potential benefits of compressor cooling. Syed M. [19] comprehensive investigation of numerical methods in simulating a steady-state vapor compression system. Xudong Wang, [20] Investigated potential benefits of compressor cooling Zubair [21] evaluated the performance of vapour Compression System and experimental investigation and theoretical study of a different type of two-stage vapor compression cascade refrigeration system. Experimental investigation and theoretical study of a different type of two-stage vapor compression cascade refrigeration system.

The above investigators did not studies the thermodynamic performances in terms of COP and exergetic efficiency and system exergy destruction ratio (EDR) for very low temperature application using ethane in the low temperature circuits and R1234ze and R1234yf in higher temperature circuit.

3. Description of four Stage Cascade Systems

The following assumptions have been taken for analyzing four stages cascade vapour compression system for low temperature applications. The cooling load is considered to be 35 "kW" Temperature of condenser is to be 70°C and temperature of ethane evaporator to be -88 °C, The temperature of high temperature evaporator to be 30 °C, temperature of secondary intermediate cascade evaporator is to be -50 °C, temperature of primary intermediate cascade evaporator is to be -10°C, temperature difference between cascade condenser and cascade evaporator is 10 °C in each stage.

4. Results and Discussions

Table-1(a) to 1(h) showing the first law efficiency of the four stage cascade refrigeration system usingR1234ze and R1234yf in the high temperature circuit and R-410a in the secondary cascade intermediate temperature circuit which is a lower temperature circuit than primary intermediate cascade circuit and ethane in the lowest temperature circuit with different thirteen ecofriendly refrigerant in primary intermediate cascade circuit. It was observed that the use of R1234ze in higher temperature circuit gives better thermodynamic performance than using R1234yf in high temperature circuit. The best combination of four stage cascade is system is to be R1234ze-R123-R410a-ethane and R1234ze-R152a-R410a-ethane. The R123 refrigerants containing chlorine and R152, R600 1nd R290 are also flammable in nature can be considered by adopting safety measures. R717 in toxic in nature. Therefore R1234ze-R134a-R410a- Ethane is most suitable for practical application.

 Table: 1(a). R1234ze in hot fluid circuit, R134a in

 secondary intermediate circuit, R404a in low temperature

 circuit and Different refrigerant in primary intermediate

 circuit

Primary Circuit Ecofriendly Refrigerant	COP _{overall}	EDR	Exergetic Efficiency
R290	0.4669	5.705	0.1491
R404A	0.4387	6.136	0.1401
R410A	0.4601	5.804	0.1470
R134A	0.4701	5.659	0.1502
R152A	0.4822	5.493	0.1540
R600	0.4799	5.523	0.1533
R600A	0.4698	5.663	0.1501
R407C	0.4385	6.14	0.1401
R507A	0.4428	6.070	0.1415
R113	0.4863	5.437	0.1553
R123	0.4873	5.424	0.1557
R717	0.4838	5.472	0.1545
R125	0.4231	6.399	0.1352

Table: 1(b). R1234ze in hot fluid circuit, R134a in
secondary intermediate circuit, R404a in low temperature
circuit and Different refrigerant in primary intermediate
circuit

		circuit		
Primary Circuit Ecofriendly Refrigerant	COP _{Hot}	COP _{inte} rmediate temperatur	COP _{inte} rmediate temperatur	COP _{low} temperature
R290	<u>circuit</u> 4.375	e circuit-ii 2.412	e circuit-II 3.829	fluid circuit 2.307
R404A	4.375	2.098	3.829	2.307
R410A	4.375	2.332	3.829	2.307
R134A	4.375	2.541	3.829	2.307
R152A	4.375	2.604	3.829	2.307
R600	4.375	2.574	3.829	2.307
R600A	4.375	2.448	3.829	2.307
R407C	4.375	2.096	3.829	2.307
R507A	4.375	2.141	3.829	2.307
R113	4.375	2.659	3.829	2.307
R123	4.375	2.672	3.829	2.307
R717	4.375	2.625	3.829	2.307
R125	4.375	1.944	3.829	2.307

 Table: 1(c). R1234yf in hot fluid circuit, R134a in

 secondary intermediate circuit, R404a in low temperature

 circuit and different refrigerant in primary intermediate

 circuit

[1		
Primary			
Circuit Ecofriendly			Exergetic
Refrigerant	COP _{overall}	EDR	Efficiency
R290	0.4543	5.891	0.1451
R404A	0.4271	6.330	0.1364
R410A	0.4478	5.991	0.1430
R134A	0.4574	5.844	0.1461
R152A	0.4691	5.674	0.1498
R600	0.4669	5.705	0.1491
R600A	0.4572	5.848	0.1460

R407C	0.4269	6.333	0.1364
R507A	0.4311	6.262	0.1377
R113	0.4731	5.618	0.1511
R123	0.474	5.604	0.1514
R717	0.4706	5.653	0.1503
R125	0.4121	6.598	0.1316

 Table: 1(d). R1234yf in hot fluid circuit, R134a in

 secondary intermediate circuit, R404a in low temperature

 circuit and Different refrigerant in primary intermediate

 circuit

Primary Circuit Ecofrien dly Refriger ant	COP _{Hot} fluid circuit	COP _{inte} rmediate temperatur e circuit-ii	COP _{inter} mediate temperature circuit-II	COP _{low} temperatu re fluid circuit
R290	3.972	2.412	3.829	2.307
R404A	3.972	2.098	3.829	2.307
R410A	3.972	2.332	3.829	2.307
R134A	3.972	2.451	3.829	2.307
R152A	3.972	2.604	3.829	2.307
R600	3.972	2.574	3.829	2.307
R600A	3.972	2.448	3.829	2.307
R407C	3.972	2.096	3.829	2.307
R507A	3.972	2.141	3.829	2.307
R113	3.972	2.659	3.829	2.307
R123	3.972	2.672	3.829	2.307
R717	3.972	2.625	3.829	2.307
R125	3.972	1.944	3.829	2.307

 Table: 1(e). R1234ze in hot fluid circuit, R134a in primary intermediate circuit, R404a in low temperature circuit, different refrigerant in primary intermediate circuit

Secondary intermediate circuit Ecofriendly Refrigerants	COP _{overall}	EDR	Exergetic Efficiency
R290	0.4701	5.659	0.1502
R404A	0.4622	5.773	0.1476
R410A	0.4701	5.659	0.1502
R134A	0.4703	5.657	0.1502
R152A	0.4720	5.633	0.1508
R600	0.4725	5.625	0.1509
R600A	0.4703	5.656	0.1502
R407C	0.4395	6.123	0.1404
R507A	0.4659	5.720	0.1488
R113	0.4742	0.5602	0.1515
R123	0.4737	0.5.609	0.1513
R717	0.4650	5.733	0.1485
R125	0.4629	5.763	0.1479

Table: 1(f). R1234ze in hot fluid circuit, R134a in primary intermediate circuit, R404a in low temperature circuit, different refrigerant in primary intermediate circuit

Secondary Intermediate Circuit Ecofriendly Refrigerants	COP _H ot fluid circuit	COP _{in} termedia te temperat ure circuit-ii	COP _{inter} mediate temperatur e circuit-II	COP _{low} temperatur e fluid circuit
R290	4.375	2.451	3.828	2.307
R404A	4.375	2.451	3.625	2.307
R410A	4.375	2.451	3.829	2.307
R134A	4.375	2.451	3.822	2.307
R152A	4.375	2.451	3.878	2.307
R600	4.375	2.451	3.894	2.307
R600A	4.375	2.451	3.834	2.307
R407C	4.375	2.451	3.116	2.307
R507A	4.375	2.451	3.717	2.307
R113	4.375	2.451	3.941	2.307
R123	4.375	2.451	3.926	2.307
R717	4.375	2.451	3.695	2.307
R125	4.375	2.451	3.642	2.307

 Table: 1(g). R1234yf in hot fluid circuit R134a in primary intermediate circuit, R404a in low temperature circuit and Different refrigerant in primary intermediate circuit

Secondary Intermediate Ecofriendly Refrigerant	COP _{overall}	EDR	Exergetic Efficiency
R290	0.4574	5.844	0.1461
R404A	0.4498	5.959	0.1437
R410A	0.4574	5.844	0.1461
R134A	0.4576	5.842	0.1462
R152A	0.4592	5.817	0.1467
R600	0.4598	5.809	0.1469
R600A	0.4577	5.841	0.1462
R407C	0.4279	6.316	0.1367
R507A	0.4533	5.906	0.1448
R113	0.4614	5.785	0.1474
R123	0.4609	5.792	0.1472
R717	0.4525	5.919	0.1445
R125	0.4505	5.949	0.1439

 Table: 1(h). R1234yf in hot fluid circuit R134a in primary intermediate circuit, R404a in low temperature circuit and Different refrigerant in primary intermediate circuit

Secondary		COP _{inte}	COP _{inte}	
intermediate	COP _H	rmediate	rmediate	COP _{low}
Ecofriendly	ot fluid	temperatur	temperatur	temperature
Refrigerant	circuit	e circuit-ii	e circuit-II	fluid circuit
R290	3.973	2.451	3.828	2.307
R404A	3.973	2.451	3.625	2.307
R410A	3.973	2.451	3.829	2.307
R134A	3.973	2.451	3.832	2.307

R152A	3.973	2.451	3.878	2.307
R600	3.973	2.451	3.894	2.307
R600A	3.973	2.451	3.834	2.307
R407C	3.973	2.451	3.116	2.307
R507A	3.973	2.451	3.717	2.307
R113	3.973	2.451	3.941	2.307
R123	3.973	2.451	3.926	2.307
R717	3.973	2.451	3.695	2.307
R125	3.973	2.451	3.642	2.307

Table: 2(a) to 2(l) Sare showing the effect of approaches (differences in temperature between cascade condenser and cascade evaporators in the various intermediate temperature circuits and low temperature circuit) on the first law and second law performances on the four stage cascade refrigeration systems. It was observed that as approach is decreasing the system first and second law efficiency is increasing and exergy destruction ratio is decreases

 Table: 2(a). R1234ze in High Temperature circuit Effect of Approach-1

Effect of Approach-1	COP _{overall}	EDR	Exergetic Efficiency
10	0.4701	5.659	0.1502
5	0.4953	5.321	0.1582
0	0.5207	5.013	0.1663

 Table: 2(b). R1234ze in High temperature circuit Effect of Approach-1

Effect				
of		COP _{inte}	COP _{inte}	
Approa		rmediate	rmediate	COPlow
ch-1	COP _{Hot}	temperatur	temperatur	temperature
	fluid circuit	e circuit-ii	e circuit-II	fluid circuit
10	4.375	2.451	3.829	2.307
5	4.375	2.783		2.307
0	4.375	3.175		2.307

 Table: 2(c). R1234ze in High temperature circuit Effect of Approach-2

Effect of Approac h -2	COP _{over}	EDR	Exergetic Efficiency
10	0.4701	5.659	0.1502
5	4920	5.364	0.1571
0	5207	5.083	0.1644

 Table: 2(d). R1234ze in High temperature circuit Effect of Approach-2

Effec t of Appr oach -2	COP _{Hot}	COP _{inter} mediate temperatur	COP _{inter} mediate temperatur	COP _{low} temperatur e
	fluid circuit	e circuit-ii	e circuit-II	fluid circuit
10	4.375	2.451	3.829	2.307
5	4.375	2.451	4.482	2.307
0	4.375	2.451	5.349	2.307

 Table: 2(e). R1234ze in High temperature circuit Effect of Approach-3

	Effect of Approach -3	COP _{overall}	EDR	Exergetic Efficiency
	10	0.4701	5.659	0.1502
ſ	5	0.4920	5.303	0.1587
	0	0.5247	4.966	0.1676

 Table: 2(f). R1234ze in High temperature circuit Effect of Approach-3

Effect of Approac h -3	COP _H ot fluid	COP _{inter} mediate temperature	COP _{inte} rmediate temperatur	COP _{low} temperature
10	circuit 4.375	circuit-ii 2.451	e circuit-II 3.829	fluid circuit 2.307
5	4.375	2.451	3.829	2.623
0	4.375	2.451	3.829	3.013

 Table: 2(g). R1234yf in High temperature circuit Effect of Approach-1

Effect of Approach-1	COP _{overall}	EDR	Exergetic Efficiency
10	0.4574	5.844	0.1461
5	0.4817	5.499	0.1539
0	0.5062	5.185	0.1617

 Table: 2(h). R1234yf in High temperature circuit Effect of Approach-1

Effect of Approac h-1	COP _{Hot} fluid	COP _{inte} rmediate temperatur	COP _{inter} mediate temperature	COP _{low} temperature
	circuit	e circuit-ii	circuit-II	fluid circuit
10	3.973	2.451	3.829	2.307
5	3.973	2.783	3.829	2.307
0	3.973	3.175	3.829	2.307

 Table: 2(i). R1234yf in High temperature circuit Effect of Approach-2

Effect of Approach-2	COP _{overall}	EDR	Exergetic Efficiency
10	0.4574	5.844	0.1461
5	0.4817	5.499	0.1539
0	0.5062	5.185	0.1617

 Table: 2(j). R1234yf in High temperature circuit Effect of Approach-2

Effect of		COP _{inte}	COP _{inter}	
Approach	COP _{Hot}	rmediate	mediate	COP _{low}
-2	fluid	temperatur	temperature	temperature
	circuit	e circuit-ii	circuit-II	fluid circuit
10	circuit 3.973	e circuit-ii 2.451	circuit-II 3.829	fluid circuit 2.307
10 5				

 Table: 2(k). R1234yf in High temperature circuit Effect of Approach-3

Effect of Approach-3	COPoverall _t	EDR	Exergetic Efficiency
10	0.4574	5.844	0.1461
5	0.4831	5.481	0.1543
0	0.5103	5.138	0.1629

Table: 2(1). R1234yf in High temperature circuit Effect of Approach-3				
Effect of Approach-3	COP _H ot fluid circuit	COP _{inte} rmediate temperatur	COP _{inter} mediate temperature	COP _{low} temperature fluid circuit
		e circuit-ii	circuit-II	
10	3.973	2.451	3.829	2.307
5	3.973	2.451	3.829	2.623
0	3.973	2.451	3.829	3.013

 Table: 3(a). Performance variation with condenser

 temperature of four stage cascade vapours compression

 refrigeration system using R1234ze in High temperature

 circuit and R404a in the low temperature circuit

Tcond			Exergetic
(°C)	COP _{overall}	EDR	Efficiency
80	0.4204	6.447	0.1343
75	0.4459	6.02	0.1424
70	0.4701	5.659	0.1502
65	0.4933	5.347	0.1576
60	0.5157	5.07	0.1647
55	0.5378	4.822	0.1718
50	0.5595	4.595	0.1787
45	0.5812	4.387	0.1856
40	0.6029	4.193	0.1926

Table: 3(b). Performance variation with condenser

 temperature of four stage cascade vapours compression

 refrigeration system using R1234ze in High temperature

 circuit and R404a in the low temperature circuit

Tcond (°C)	COP _{Hot} fluid circuit	COP _{int} ermediate temperatu re circuit- ii	COP _{inter} mediate temperature circuit-II	COP _{low} temperature fluid circuit
80	3.054	2.451	3.829	2.307
75	3.651	2.451	3.829	2.307
70	4.375	2.451	3.829	2.307
65	5.282	2.451	3.829	2.307
60	6.467	2.451	3.829	2.307
55	8.10	2.451	3.829	2.307
50	10.52	2.451	3.829	2.307
45	14.52	2.451	3.829	2.307
40	22.47	2.451	3.829	2.307

Table: 3(c). Performance variation with condenser temperature of four stage cascade vapours compression refrigeration system using R1234yf in High temperature circuit and R404a in the low temperature circuit

Tcond (°C)	COP_overal	System EDR	Exergetic Efficiency
80	0.3945	6.935	0.1260
75	0.4279	6.316	0.1367
70	0.4574	5.844	0.1461
65	0.4844	5.463	0.1547
60	0.5096	5.143	0.1628
55	0.5337	4.866	0.1705
50	0.5569	4.622	0.1779
45	0.5796	4.401	0.1851
40	0.6021	4.20	0.1923

 Table: 3(d). Performance variation with condenser

 temperature of four stage cascade vapours compression

 refrigeration system using R1234yf in High temperature

 circuit and R404a in the low temperature circuit

Tcond		COP _{inte}	COP _{inte}	
(°C)	COP _{Hot}	rmediate	rmediate	COP _{low}
	fluid	temperatur	temperatur	temperature
	circuit	e circuit-ii	e circuit-II	fluid circuit
80	2.573	2.451	3.829	2.307
75	3.216	2.451	3.829	2.307
70	3.973	2.451	3.829	2.307
65	4.904	2.451	3.829	2.307
60	6.106	2.451	3.829	2.307
55	7.748	2.451	3.829	2.307
50	10.17	2.451	3.829	2.307
45	14.14	2.451	3.829	2.307
0.1923	22.02	2.451	3.829	2.307
From '	Tables_3. i	t was obse	erved that	as condens

From Tables-3: it was observed that as condenser temperature decreases overall COP of system (First law efficiency of system) increases and System EDR is decreases and also second law efficiency (exergetic efficiency) increases. While First law efficiency of hot fluid circuit is increases. There will not be effect on other circuit first law efficiencies. The exergetic efficiency and Overall COP of system using R1234ze is higher than using R1234yf in the high temperature circuit while system EDR increases. As decreasing High temperature evaporator temperature, the first law efficiency (i.e. overall cop of system) and second law efficiency (i.e. exergetic efficiency of whole system) is is increasing up to maximum value at the evaporator temperature of 25°C and then decreases rapidly.

As decreasing High temperature evaporator temperature the system EDR first decreasing up to decreasing evaporator temperature and then further constant and then increasing and optimum becomes at evaporator temperature at 25°C in both cases using R1234yf and R1234ze in the high temperature circuit. However Cop of hot fluid circuit is decreases and COP of primary intermediate fluid circuit is increases.

Table: 4(a). Performance variation with evaporator temperature in the high temperature circuit of Four stage cascade vapour compression refrigeration system using R1234ze in High temperature circuit and R404a in the low

temperature circuit

Tevaporator High temp circuit (°C)	COP Overall	System EDR	Exergetic Efficiency
50	0.4331	6.229	0.1383
45	0.4476	5.995	0.1430
40	0.4584	5.829	0.1464
35	0.4659	5.720	0.1488
30	0.4701	5.659	0.1502
25	0.4713	5.642	0.1505
20	0.4696	5.666	0.150
15	0.4652	5.729	0.1486
10	0.4583	5.831	0.1464
5	0.4489	5.974	0.1434
0	0.4375	6.158	0.1397

Table: 4(b). Performance variation with evaporator temperature in the high temperature circuit of four stage

cascade vapour compression refrigeration system using R1234ze in High temperature circuit and R404a in the low temperature circuit

Tevapora tor High temp circuit	COP Hot fluid	COP _{inte} rmediate temperatur	COP _{interm} ediate temperature	COP _{low} temperature
(°C)	circuit	e circuit-ii	circuit-II	fluid circuit
50	10.53	1.489	3.829	2.307
45	8.06	1.61	3.829	2.307
40	6.417	1.914	3.829	2.307
35	5.248	2.165	3.829	2.307
30	4.375	2.451	3.829	2.307
25	3.699	2.783	3.829	2.307
20	3.161	3.175	3.829	2.307
15	2.723	3.646	3.829	2.307
10	2.361	4.229	3.829	2.307
5	2.056	4.97	3.829	2.307
0	1.791	5.951	3.829	2.307

Table: 4(c). Performance variation with evaporatortemperature in the high temperature circuit temperature offour stage cascade vapour compression refrigeration systemusing R1234yf in High temperature circuit and R404a in thelow temperature circuit

Tevaporator High temp circuit (°C)	COP_O verall	EDR	Exergetic Efficiency
50	0.4291	6.295	0.1371
45	0.4419	6.085	0.1412
40	0.4507	5.946	0.1440
35	0.4559	5.868	0.1456
30	0.4574	5.844	0.1461
25	0.4557	5.870	0.1456
20	0.4507	5.946	0.1440
15	0.4428	6.070	0.1414
10	0.4321	6.245	0.1380
5	0.4189	6.474	0.1338
0	0.4033	6.762	0.1288

 Table: 4(d). Performance variation with evaporator

 temperature in the high temperature circuit temperature of
 four stage cascade vapour compression refrigeration system

 using R1234yf in High temperature circuit and R404a in the
 low temperature circuit

Tevaporat				COPlow
or High		COP _{inte}	COP _{inte}	temperatu
temp	COP _H	rmediate	rmediate	re
circuit (°C)	ot fluid	temperatur	temperatur	fluid
	circuit	e circuit-ii	e circuit-II	circuit
50	9.804	1.489	3.829	2.307
45	7.462	1.690	3.829	2.307
40	5.906	1.914	3.829	2.307
35	4.799	2.165	3.829	2.307
30	3.973	2.451	3.829	2.307
25	3.333	2.783	3.829	2.307
20	2.825	3.175	3.829	2.307
15	2.413	3.646	3.829	2.307
10	2.072	4.229	3.829	2.307
5	1.786	4.970	3.829	2.307
0	1.544	5.951	3.829	2.307

As evaporator temperature decreases, the first law efficiency (overall COP) and second law efficiency (exergetic efficiency) of the system is increases and maximum efficiency is obtained at evaporator temperature of -10 $^{\circ}$ C and also cop of primary intermediate temperature circuit is decreases and secondary intermediate temperature circuit COP is increases.

Table: 5(a). Performance variation with cascade evaporator

 temperature in the primary intermediate temperature circuit

temperature of four stage cascade vapour compression refrigeration system using R1234ze in High temperature

circuit and R404a in the low temperature circuit

Tevaporat			Exergetic
or (°C)	COP _{overall}	EDR	Efficiency
20	0.4436	6.057	0.1417
15	0.4546	5.886	0.1452
10	0.4633	5.757	0.1480
5	0.4696	5.666	0.150
0	0.4738	5.607	0.1513
-5*	0.4758	5.579	0.1520
-10*	0.4759	5.579	0.1520
-15	0.4739	5.609	0.1514
-20	0.4701	5.659	0.1502
-25	0.4646	5.739	0.1484
-30	0.4573	5.485	0.1461
-35	0.4485	5.980	0.1433
-40	0.4383	6.143	0.140

Table: 5(b). Performance variation with cascade evaporator temperature in the primary intermediate temperature circuit temperature of four stage cascade vapour compression refrigeration system using R1234ze in High temperature

circuit and R404a in the low temperature circuit

Teva		COP _{inter}	COP _{inte}	
porat		mediate	rmediate	COP _{low}
or	COP _{Hot}	temperatur	temperatur	temperature
(°C)	fluid circuit	e circuit-ii	e circuit-II	fluid circuit
20	4.375	10.33	1.460	2307
15	4.375	7.951	1.629	2307
10	4.375	6.367	1.818	2307
5	4.375	5.239	2.032	2307
0	4.375	4.396	2.278	2307
-5*	4.375	3.744	2.565	2307
-10*	4.375	3.224	2.905	2307
-15	4.375	2.801	3.317	2307
-20	4.375	2.451	3.829	2307
-25	4.375	2.157	4.482	2307
-30	4.375	1.907	5.349	2307
-35	4.375	1.691	6.559	2307
-40	4.375	1.505	8.368	2307

 Table: 5(c). Performance variation with cascade evaporator

 temperature in the primary intermediate temperature circuit

 temperature of four stage cascade vapour compression

 refrigeration system using R1234yf in High temperature

 circuit and R404a in the low temperature circuit

Tevaporat or (°C)	COP _{overall}	EDR	Exergetic Efficiency
20	0.4319	6.249	0.1379
15	0.4425	6.075	0.1413

10	0.4509	5.944	0.1440
5	0.4570	5.851	0.1460
0	0.4610	5.791	0.1473
-5*	0.4630	5.762	0.1479
-10*	0.4630	5.762	0.1479
-15	0.4611	5.789	0.1473
-20	0.4574	5.844	0.1461
-25	0.4521	5.925	0.1444
-30	0.4451	6.034	0.1422
-35	0.4366	6.170	0.1395
-40	0.4267	6.336	0.1363

 Table: 5(d). Performance variation with cascade evaporator

 temperature in the primary intermediate temperature circuit

 temperature of four stage cascade vapour compression

 refrigeration system using R1234yf in High temperature

 circuit and R404a in the low temperature circuit

Teva porat or (°C)	COP _{Hot} fluid circuit	COP _{inter} mediate temperatur e circuit-ii	COP _{inte} rmediate temperatur e circuit-II	COP _{low} temperature fluid circuit
20	4.375	10.33	1.460	2307
15	4.375	7.951	1.629	2307
10	4.375	6.367	1.818	2307
5	4.375	5.239	2.032	2307
0	4.375	4.396	2.278	2307
-5*	4.375	3.744	2.565	2307
-10*	4.375	3.224	2.905	2307
-15	4.375	2.801	3.317	2307
-20	4.375	2.451	3.829	2307
-25	4.375	2.157	4.482	2307
-30	4.375	1.907	5.349	2307
-35	4.375	1.691	6.559	2307
-40	4.375	1.505	8.368	2307

 Table: 6(a). Performance variation with cascade evaporator temperature in the secondary intermediate temperature circuit temperature of four stage cascade vapour compression refrigeration system using R1234ze in High temperature circuit and R404a in the low temperature circuit

Tevapor ator (°C)	COP overall	EDR	Exergetic Efficiency
-70	0.4631	5.76	0.1479
-65	0.4674	5.697	0.1493
-60	0.4701	5.66	0.1502
-55***	0.4710	5.647	0.1504
-50	0.4701	5.659	0.1502
-45	0.4675	5.696	0.1493
-40	0.4631	5.760	0.1479
-35	0.4569	5.851	0.1460
-30	0.4490	5.973	0.1434

 Table: 6(b). Performance variation with cascade evaporator

 temperature in the secondary

 intermediate temperature

 circuit temperature of four stage cascade vapour

compression refrigeration system using R1234ze in High temperature circuit and R404a in the low temperature circuit

Tevap orator (°C)	COP _{Hot} fluid	COP _{inte} rmediate temperatur	COP _{inter} mediate temperatur	COP _{low} temperature
	circuit	e circuit-ii	e circuit-II	fluid circuit
-70	4.375	2.451	2.116	4.161
-65	4.375	2.451	2.426	3.508
-60	4.375	2.451	2.798	3.013
-55***	4.375	2.451	3.255	2.603
-50	4.375	2.451	3.829	2.307
-45	4.375	2.451	4.568	2.046
-40	4.375	2.451	5.556	1.825
-35	4.375	2.451	6.942	1.636
-30	4.375	2.451	9.022	1.42

As increasing evaporator temperature overall cop is increases while System EDR first decreases while second law efficiency is increases. The maximum efficiency was obtained at -55 oC and then decreases as increasing evaporator temperature. Secondary intermediate circuit COP is increases while low temperature circuit COP is decreases. Table-6(b): Performance variation with cascade evaporator temperature in the secondary intermediate temperature circuit temperature of four stage cascade vapour compression refrigeration system using R1234yf in High temperature circuit and R404a in the low temperature circuit

 Table: 6(c). Performance variation with cascade evaporator

 temperature in the secondary intermediate temperature

 circuit temperature of four stage cascade vapour

compression refrigeration system using R1234yf in High temperature circuit and R404a in the low temperature circuit

Tevaporator (°C)	COP _{overall}	EDR	Exergetic Efficiency
-70	0.4507	5.946	0.1440
-65	0.4549	5.883	0.1453
-60	0.4574	5.845	0.1461
-55***	0.4583	5.831	0.1464
-50	0.4574	5.844	0.1461
-45	0.4949	5.882	0.1453
-40	0.4507	5.946	0.1440
-35	0.4447	6.039	0.1421
-30	0.4370	6.163	0.1396

 Table: 6(d). Performance variation with cascade evaporator temperature in the secondary intermediate temperature circuit temperature of four stage cascade vapour compression refrigeration system using R1234yf in High temperature circuit and R404a in the low temperature circuit

Teva porat or (°C)	COP _{Hot} Auid circuit	COP _{inter} mediate temperatur e circuit-ii	COP _{inter} mediate temperatur e circuit-II	COP _{low} temperature fluid circuit
-70	0.3973	2.451	2.116	4.161
-65	0.3973	2.451	2.426	3.508
-60	0.3973	2.451	2.798	3.013
-55*	0.3973	2.451	3.255	2.603
-50	0.3973	2.451	3.829	2.307
-45	0.3973	2.451	4.568	2.046
-40	0.3973	2.451	5.556	1.825
-35	0.3973	2.451	6.942	1.636
-30	0.3973	2.451	9.022	1.42

Table: 7(a). Performance variation with low temperature evaporator temperature in the of four stage cascade vapour compression refrigeration system using R1234ze in High temperature circuit and R404a in the low temperature circuit

Tevaporat or (°C)	COP _{overall}	EDR	Exergetic Efficiency
-90	0.4701	5.659	0.1502
-85	0.5024	5.14	0.1629
-80	0.5358	4.676	0.1762
-75	0.5701	4.259	0.1902
-70	0.6056	3.884	0.2048
-65	0.6421	3.546	0.220
-60	0.6796	3.239	0.2359
-55	0.7181	2.962	0.2524

Table: 7(b). Performance variation with low temperature evaporator temperature in the of four stage cascade vapour compression refrigeration system using R1234ze in High temperature circuit and R404a in the low temperature circuit

Tevapo rator		COP _{inte}	COP _{inter}	COP _{low}
(°C)	COP _{Hot}	rmediate temperatur	mediate temperature	temperature
	fluid circuit	e circuit-ii	circuit-II	fluid circuit
-90	4.375	2.451	3.829	2.307
-85	4.375	2.451	3.829	2.697
-80	4.375	2.451	3.829	3.185
-75	4.375	2.451	3.829	3.812
-70	4.375	2.451	3.829	4.645
-65	4.375	2.451	3.829	5.804
-60	4.375	2.451	3.829	7.525
-55	4.375	2.451	3.829	10.35

Table: 7(c). Performance variation with low temperature evaporator temperature in the of our stage cascade vapour

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compression refrigeration system using R1234yf in High temperature circuit and R404a in the low temperature circuit

Tevaporator			Exergetic
(°C)	COPoverall	EDR	Efficiency
-90	0.4574	5.844	0.1461
-85	0.4881	5.314	0.1584
-80	0.5207	4.840	0.1712
-75	0.5538	4.415	0.1847
-70	0.5878	4.032	0.1987
-65	0.6228	3.686	0.2134
-60	0.6587	3.373	0.2287
-55	0.6956	3.09	0.2445

Table: 7(d). Performance variation with low temperature evaporator temperature in the of four stage cascade vapour compression refrigeration system using R1234yf in High temperature circuit and R404a in the low temperature circuit

Teva		COP _{inter}	COP _{inte}	
porat	~~~	mediate	rmediate	COP _{low}
or	COP _{Hot}	temperatur	temperatur	temperature
(°C)	fluid circuit	e circuit-ii	e circuit-II	fluid circuit
-90	3.972	2.451	3.829	2.307
-85	3.972	2.451	3.829	2.697
-80	3.972	2.451	3.829	3.185
-75	3.972	2.451	3.829	3.812
-70	3.972	2.451	3.829	4.645
-65	3.972	2.451	3.829	5.804
-60	3.972	2.451	3.829	7.525
-55	3.972	2.451	3.829	10.35

Table-7(a) to 7(d) are showing the effect of low temperature evaporator on the system first and second law performances and system exergy destruction ratio and various circuit first law performances . as low temperature evaporator temperature is decreasing , the first law and second law efficiencies are increasing and exergy destruction ratio is decreasing and high temperature circuit first law performances in increasing.

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